

Subject Code.....

ROLL NO.....

**SEMESTER EXAMINATION 2022-23**

**1<sup>st</sup> year M.Tech. Thermal Engineering**

**Convective Heat Transfer (TET-303)**

**Duration : 3 hrs**

**Max. Marks: 100**

**Note:- Attempt all questions. All question carry equal marks. In case any ambiguity or missing data, the same may be assumed and state the assumption made in the answer.**

<b>Q.1.</b>	<b>Answer any four parts of the following.</b>	<b>5×4=20</b>
	<p>a) What is the natural convection? How does it differ from the forced convection? What force causes natural convection currents?</p> <p>b) Discuss laminar sublayer, buffer layer and turbulent layer in a boundary layer?</p> <p>c) What do you understand by hydrodynamically developed flow in a circular tube?</p> <p>d) What do you mean by hydro dynamically developed flow in a circular tube? Explain.</p> <p>e) What is the natural convection? How does it differ from the forced convection? What force causes natural convection currents?</p> <p>f) What do you understand by local and average value of heat transfer coefficient?</p>	
<b>Q.2.</b>	<b>Answer any four parts of the following.</b>	<b>5×4=20</b>
	<p>a) Explain the Reynold Colburn analogy for laminar flow over plate.</p> <p>b) Discuss in details, the various regimes of pool boiling.</p> <p>c) Drive the energy equation for the laminar boundary layer over a flat plate.</p> <p>d) Define Nusselt number and discuss its significance.</p> <p>e) What property is responsible for development of velocity boundary layer? What property is for thermal boundary layer?</p> <p>f) Show that the coefficient of volumetric expansion for an ideal gas is <math>\beta = 1/T</math>, where T is absolute temperature of gas.</p>	
<b>Q.3.</b>	<b>Attempt any two parts of the following.</b>	<b>10×2=20</b>
	<p>a) Distinguish between</p> <p>I. Subcooled and saturated boiling</p>	

	<p>II. Nucleate and film boiling</p> <p>b) Water at 20<sup>0</sup>C flows through a small tube, 1mm in diameter at a uniform speed of 0.2 m/s. The flow is fully developed at a point beyond which a constant heat flux of 6000 W/m<sup>2</sup> is imposed. How much farther down the tube will the water reach 74<sup>0</sup>C as its hottest point?</p> <p>Take the physical properties of water at 320K</p> <p><math>\rho = 989 \text{ kg/m}^3</math>, <math>C_p = 4180 \text{ J/kg.K}</math>, <math>\mu = 577 \times 10^{-6}</math></p> <p><math>k_f = 0.640 \text{ W/m.K}</math>, <math>Pr = 3.77</math></p> <p>c) Drive an equation for energy for flow over a flat plate.</p>	
<b>Q.4.</b>	<b>Attempt any two parts of the following.</b>	<b>10×2=20</b>
	<p>a) Discuss the condition under which the dropwise condensation can take place. Why the rate of heat transfer in dropwise condensation is many times that of filmwise condensation.</p> <p>b) Why is the flow separation in flow over cylinders delayed in turbulent?</p> <p>c) Vertical door of a hot oven is 0.5 m high and is maintained at 200<sup>0</sup>C. It is exposed to atmospheric air at 20<sup>0</sup>C. Find (a) local heat transfer coefficient half way up the door; (b) average heat transfer coefficient for entire door; (c) thickness of free convection boundary layer at the top of the door. Take properties of atmospheric air at 110<sup>0</sup>C</p> <p><math>\rho = 0.922 \text{ kg/m}^3</math>, <math>C_p = 1000 \text{ J/kg.K}</math>, <math>\mu = 2.24 \times 10^{-5} \text{ kg/ms}</math></p> <p><math>\nu = 2.429 \times 10^{-5} \text{ m}^2/\text{s}</math>, <math>k_f = 0.0332 \text{ W/m.K}</math>, <math>Pr = 0.687</math></p>	
<b>Q.5.</b>	<b>Attempt any two parts of the following.</b>	<b>10×2=20</b>
	<p>a) The steam condenses on a vertical plane wall, derive expression for the followings.</p> <p>I. Average heat transfer coefficient,</p> <p>II. film thickness</p>	

III. rate of condensation and

IV. rate of heat flow

- b) Drive the log mean temperature difference for fully developed heat transfer?
- c) In a constant surface temperature tube, the fluid enters at temperature  $T_i$  and leaves the tube at temperature  $T_o$ . Prove that

$$\frac{T_s - T_o}{T_s - T_i} = \exp\left(-\frac{hA_s}{mC_p}\right)$$